

^{END} B₃ exhaust gas downstream side, and the other one is closed by a plug on the exhaust gas upstream side.

Page 6, lines 29-35, delete current paragraph and insert therefor:

B⁴ In this embodiment, the NO oxidation catalyst and NO₂ decomposition catalyst of the invention reside as a coated layer covering the wall columns of the filter. In the coated layer, the NO oxidation catalyst and NO₂ decomposition catalyst may reside in a randomly mixed state as shown in Fig. 2(a), or they may reside in layers as shown in Fig. 2(b).

Page 7, lines 2-10, delete current paragraph and insert therefor:

B⁵ Tungstic acid/zirconia (WO₃/ZrO₂), silica, silica-alumina, MFI zeolite (SiO₂/Al₂O₃ = 40), dealuminized Y zeolite (SiO₂/Al₂O₃ = 200), γ -alumina, zirconia and Ba/ γ -alumina were prepared as carriers, and after coating each of the carriers onto monolith substrates, each carrier was impregnated with a dinitrodiamine Pt solution and subjected to drying and pre-firing followed by 1 hour of firing at 650°C to obtain catalysts with 2 g of Pt loaded on each carrier per liter volume of substrate.

Page 7, table 1, delete current table and insert therefor:

Table 1 Comparison of NO oxidation performance

B⁶

Catalyst carrier	NO oxidation rate (%)	
	200°C	250°C
WO ₃ /ZrO ₂	64	93
Silica	45	92
Silica-alumina	34	92
MFI zeolite	66	92
Y zeolite	62	93
γ -alumina	15	90
Zirconia	17	90
Ba/ γ -alumina	8.5	20

Catalyst component: 2 g Pt/1L filter

Page 8, lines 25-28, delete current paragraph and insert therefor:

B⁷ The resulting slurry was coated and dried onto a filter substrate, and then fired at 650°C for 1 hour to form a layer containing WO₃/ZrO₂ powder and Ba/γ-alumina powder on the filter substrate.

Page 8, lines 29-34, delete current paragraph and insert therefor:

B Next, the layer was impregnated with a dinitrodiamine Pt aqueous solution, and then further impregnated with a Rh nitrate aqueous solution and fired at 500°C for 1 hour to obtain a catalyst according to the invention carrying 2 g of Pt and 0.1 g of Rh per liter of filter substrate.

Page 9, lines 14-17, delete current paragraph and insert therefor:

B⁹ The resulting slurry was coated and dried onto a filter substrate, and then fired at 650°C for 1 hour to form a layer containing WO₃/ZrO₂ powder and Fe/γ-alumina powder on the filter substrate.

Page 9, lines 18-23, delete current paragraph and insert therefor:

B¹⁰ Next, in the same manner as Example 1, the layer was impregnated with a dinitrodiamine Pt aqueous solution, and then further impregnated with a Rh nitrate aqueous solution and fired at 500°C for 1 hour to obtain a catalyst according to the invention carrying 2 g of Pt and 0.1 g of Rh per liter of filter substrate.

Page 10, lines 2-4, delete current paragraph and insert therefor:

B¹¹ The resulting slurry was coated and dried onto a filter substrate, and then fired at 650°C for 1 hour to form a layer containing Ba/γ-alumina powder.

Page 10, lines 5-10, delete current paragraph and insert therefor:

Next, the layer was impregnated with a dinitrodiamine Pt aqueous solution, and then further impregnated with a Rh nitrate aqueous solution and fired at 500°C for 1 hour to obtain a comparison catalyst carrying 2 g of Pt and 0.1 g of Rh per liter of filter substrate.

Page 10, lines 19-21, delete current paragraph and insert therefor:

¹²
B The resulting slurry was coated and dried onto a filter substrate, and then fired at 650°C for 1 hour to form a layer containing silica powder.

Page 10, lines 22-27, delete current paragraph and insert therefor:

¹³
B Next, the layer was impregnated with a dinitrodiamine Pt aqueous solution, and then further impregnated with a Rh nitrate aqueous solution and fired at 500°C for 1 hour to obtain a comparison catalyst carrying 2 g of Pt and 0.1 g of Rh per liter of filter substrate.

Page 10, line 34- page 11, lines 1-10, delete current paragraph and insert therefor:

¹⁴
B The proportion of NO₂ decomposed to NO by the catalysts of Examples 1-2 and Comparative Examples 1-2 above was measured using diesel engine exhaust gas. Lean (air/fuel ratio = 30) and rich (air/fuel ratio = 14) operating conditions were employed, repeatedly alternated for 30 seconds and 1 second, respectively, and the NO₂ decomposition rate was measured based on the exhaust gas composition shown below, under lean conditions. The results are shown in Table 2. For the catalyst of Comparative Example 2, there was provided a particulate matter-accumulated filter (without catalyst) downstream from the catalyst, and the NO₂ decomposition rate as measured at the outlet port of the filter.

Page 11, table 2, delete current table and insert therefor:

Table 2 Comparison of NO₂ decomposition performance

	Catalyst		NO ₂ decomposition rate (%)	
	NO oxidation catalyst	NO ₂ decomposition catalyst	200°C	250°C
Example 1	Pt/WO ₃ /ZrO ₂	Pt/Ba/γ-alumina	85	94
Example 2	Pt/WO ₃ /ZrO ₂	Fe/γ-alumina	88	90
Comp. Ex.1	Pt/Ba/γ-alumina		78	88
Comp. Ex.2	Upstream Pt/silica + monolith filter		2.1	3.5

Catalyst components: (2 g Pt + 0.1 g Rh)/1L filter

Page 11, lines 17-27, delete current paragraph and insert therefor: